Diversity and Ecophysiology of New Isolates of Extremely Acidophilic CS₂-Converting Acidithiobacillus Strains

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Biofiltration of industrial carbon disulfide (CS₂)-contaminated waste air streams results in the acidification of biofilters and therefore reduced performance, high water use, and increased costs. To address these issues, we isolated 16 extremely acidophilic CS₂-converting Acidithiobacillus thiooxidans strains that tolerated up to 6% (vol/vol) sulfuric acid. The ecophysiological properties of five selected strains (2Bp, Sts 4-3, S1p, G8, and BBW1) were compared. These five strains had pH optima between 1 (2Bp) and 2 (S1p). Their affinities for CS₂ ranged between 80 (G8) and 130 (2Bp) µM. Strains S1p, G8, and BBW1 had more hydrophobic cell surfaces and produced less extracellular polymeric substance than did strains 2Bp and Sts 4-3. All five strains converted about 80% of the S added as CS₂ to S⁰ when CS₂ was supplied in excess. The rate of S⁰ consumption varied between 7 (Sts 4-3) and 63 (S1p) nmol O₂ min⁻¹ ml culture⁻¹. Low S⁰ consumption rates correlated partly with low levels of cell attachment to externally produced S⁰ globules. During chemostat growth, the relative amount of CS₂ hydrolase in the cell increased with decreasing growth rates. This resulted in more S⁰ accumulation during CS₂ overloads at low growth rates. Intermittent interruptions of the CS₂ supply affected all five strains. Strains S1p, G8, and BBW1 recovered from 24 h of starvation within 4 h, and strains 2Bp and Sts 4-3 recovered within 24 h after CS₂ was resupplied. We recommend the use of mixtures of Acidithiobacillus strains in industrial biofilters.

Carbon disulfide (CS₂) is a toxic, volatile, flammable, and explosive solvent widely used in, e.g., the viscose rayon industry (1). Because of its toxicity and the increasingly stringent rules governing the emission of harmful gases, it is necessary to treat CS₂-containing industrial waste gases. Biological treatment of CS₂ (and hydrogen sulfide, H₂S) with sulfur-oxidizing bacteria provides an attractive alternative to conventional treatment systems (e.g., active carbon, incineration, caustic scrubbing) (2,3). Typical concentrations of CS₂ in contaminated air from viscose industries are around 4 to 20 nmol ml⁻¹ (100 to 500 ppm) (2).

The number of microorganisms known to be able to grow chemolithoautotrophically on CS₂ is limited to some Thiobacillus species, Thiothrix ramosa, Paracoccus denitrificans, and a Thiomonas sp. (4–8). All of these CS₂-utilizing bacteria grow at neutral pH. Thus far, only one CS₂-utilizing species (Thiobacillus sp. strain TJ330, DSM8985) capable of growth under acidic conditions (as low as pH 0.5) has been described (9). The only reported screening of 10 (Acidithiobacillus) strains showed that CS₂ conversion is not a general trait of (acid)thiobacilli (4). In that screening, only one strain, Thiobacillus thioparus TK-m, was found to be capable of CS₂ conversion. We recently discovered that CS₂ conversion is not limited to the domain Bacteria; the hyperthermophilic archaea Acididanus sp. strain A1-3 and Sulfolobus solfataricus P2 can also grow on CS₂ as a main carbon and energy source (10). However, these archaea are not able to grow at the extremely low pH values that acidithiobacilli can cope with. CS₂-converting sulfur oxidizers in operating biofilters are also acidophilic bacteria (2,11–13). They convert CS₂ via the two hydrolysis reaction steps CS₂ + H₂O → COS + H₂S and COS + H₂O → CO₂ + H₂S and obtain their energy from the oxidation of H₂S via S⁰ and SO₂⁻ → SO₄²⁻ as follows: H₂S + SO₂⁻ → SO₄²⁻ + 2H⁺ (14). Therefore, an inherent result of CS₂ conversion is acidification of the biofilters, which can be limited only by flushing the trickling filters with fresh water. Operating at a pH as low as possible will considerably reduce the volume of fresh water used for neutralization. Water use would be further reduced if the H₂SO₄ produced could be reused in the viscose-rayon industry. This becomes economically feasible when the H₂SO₄ concentration in the reactor effluent is at least 10% (wt/vol) (5.6% [vol/vol]). However, the performance of biotrickling filters is compromised by severe acidification and buildup of elemental sulfur (S⁰) that can clog the filters. Therefore, we set out to isolate new CS₂-converting bacterial strains able to tolerate extremely low pH values with variable CS₂ loads without loss of CS₂ conversion efficiency and without the production of large amounts of elemental sulfur.

MATERIALS AND METHODS

Media and culture conditions. Strains were enriched and cultured in basal salt mineral medium (MM) with CS₂ as the sole carbon and energy source as described previously (15). Bacteria were grown at room temperature (RT, 22°C) in 120-ml bottles containing 20 ml MM acidified with sulfuric acid. Alternatively, bacteria were grown on MM plates solidified with 1% (vol/vol) Gelrite (16) and acidified with 0.1% (vol/vol) sulfuric acid. This was the maximum [H₂SO₄] at which plates could still be poured without the Gelrite solution immediately solidifying when brought into contact with the H₂SO₄-containing MM solution. In the case of Gelrite, H₂SO₄ increases solidification while the opposite occurs with agar (ose). Plates were incubated in an airtight jar. Unless stated differently, sulfuric acid concentrations are reported as percentages (vol/vol) (1% [vol/vol] is 001).
equivalent to 1.8% [wt/vol] and 0.18 M sulfuric acid). Strains were also grown in minichemostat reactors as described previously (15).

The headspaces of the bottles and jars used were continuously flushed with a CS₂-containing air stream from a purpose-built distribution system (see the supplemental material).

**Enrichment and isolation.** Volumes of 0.5 to 1 ml of environmental or industrial samples were inoculated into 120-ml serum bottles with 20 ml acidified MM. The initial H₂SO₄ concentration was 0.5 to 1% [vol/vol] in the environmental samples and 2% in the samples from the biotrickling filters. CS₂ was supplied as the sole energy source via the distribution system. When a visually dense culture was observed, the enrichment was transferred to fresh MM. The maximum H₂SO₄ concentration at which growth occurred was determined by the subsequent transfer of enrichments to MM with higher H₂SO₄ concentrations. Pure cultures were obtained from enrichment cultures grown in 4 to 6% H₂SO₄ on Gelrite plates. Single colonies were serially transferred three times to fresh plates and checked microscopically for purity. Fungal contamination (present mainly in the enrichments from industrial samples) was eliminated by adding 150 μg ml⁻¹ chlorothalonil either to the plates or to liquid cultures. The H₂SO₄ tolerance of each isolated strain was confirmed by repeated subculturing at least three times in liquid MM containing 4 to 5% H₂SO₄.

**Screening of known Acidithiobacillus strains for CS₂ conversion capacity.** Five Acidithiobacillus strains were obtained from the Deutsche Sammlung von Mikroorganismen und Zellkulturen (DSMZ) and grown in batch cultures in the media suggested (DSMZ medium number in parentheses after the strain name) or as otherwise stated, i.e., *A. ferrooxidans* DSM14882 (882), *A. caldus* DSM8584 (150a), *A. thiooxidans* DSM14887 (71), *A. thiooxidans* DSM504 (MM plus 10 g liter⁻¹ sterile S0), and *A. albertensis* DSM14366 (71). After growth for 1 week, the headspace of the cultures was supplemented with CS₂ (20 to 30 nmol ml⁻¹). The CS₂ concentration and the presence of intermediates (H₂S and COS) in the headspace were monitored over time by gas chromatography (17).

**PCR, cloning, and sequencing.** DNA was isolated from each strain by phenol extraction (18). The 16S rRNA gene and the 16S-23S intergenic spacer region (ISR) of 16 isolated CS₂-hydrolyzing bacterial strains were amplified by hot-start PCR with the Go Taq Green buffer system (Fermentas) with 2.5 mM MgCl₂, 0.2 mM deoxynucleoside triphosphates, 1 μl bovine serum albumin, 0.4 μM each primer (see Table S1 in the supplemental material), and 1 μl Taq polymerase (Fermentas). The PCR protocol consisted of 2 min at 95°C, 30 cycles of 1 min at 95°C, 1 min at 54 to 65°C, and 2 min at 72°C, and a final elongation step of 10 min at 72°C. PCR products were ligated into pGem-T Easy (Promega) and transformed into *Escherichia coli* strain TOP10 (Invitrogen) according to the manufacturer's instructions. Plasmids with a correct insert were Sanger sequenced by the following method (19) in MEGA 4.0.20 with the following settings: maximum composite likelihood nucleotide substitution model, gaps and missing data eliminated, transitions and transversions included, uniform rates among sites, and homogeneous pattern among lineages. Sequences of the ribosomal operon of *A. thiooxidans* ATCC 19377 and *A. caldus* ATCC 51756 were kindly made available by Jorge Valdés and David Holmes, CBGB, Santiago, Chile (21).

**Cryo-SEM.** Cryo-scanning electron microscopy (cryo-SEM) was used to study the morphology of colonies growing on 1% Gelrite plates acidified with 0.018 M H₂SO₄ by a method similar to that described in reference 22. Blocks containing colonies were cut out of the Gelrite, mounted on electroconductive aqueous colloidal graphite (DAG; Agar Scientific) on a mounting stub, and quickly frozen by submersion in degassed liquid N₂ (−196°C). While under vacuum, the sample was transferred to the Gatan cryotransfer box. Sections through colonies were made with a razor blade at this stage when required. The temperature was subsequently increased to −100°C to sublime off water that had settled on top of the specimen by condensation for a period of 5 min. When all of the surface water had been removed, the temperature was reduced to between −100 and −150°C. The sample was then sputter coated for 45 s with a mixture of 60% gold and 40% palladium and transfered to a JEOL 6330F scanning electron microscope.

**Yield determinations.** For total carbon measurements, 3- to 4-ml reactor samples were centrifuged and the pellets were resuspended in 2 ml mM HCl, pH 3. The washed cells were dried overnight under vacuum at 70°C. The C/N ratio of the dried material (0.3 to 0.4 mg) was determined by elemental analysis with a Thermo Fisher Scientific EA 1110 CHN element analyer coupled to a Finnigan DELTAplus mass spectrometer. For protein determinations, 2-ml reactor samples were centrifuged at 4°C for 30 min at 18,000 × g. The pellets were resuspended in 0.5 ml 1 mM NaOH, boiled for 5 min, and neutralized with 0.5 ml 1 M HCl. Alternatively, 0.5 ml 1 M NaOH was added directly to 200-μl reactor samples, and after boiling, the mixture was neutralized with 0.3 ml 1 M HCl. Protein concentrations were determined with the Bio-Rad protein assay kit according to the manufacturer's instructions. Culture density, determined by both cell density and the presence of S0, was measured spectrophotometrically as the optical density at 600 nm (OD₆₀₀).

**Determination of pH optima.** pH optima were determined by a floating-filter method. Samples taken from the steady-state chemostats (1% H₂SO₄ measured pH, 0.72) were diluted 10⁶-fold in MM at pH 2, and 1 ml of this dilution was filtered through a sterile, 0.2-μm, 25- or 47-mm-diameter Cycloprene polycarbonate filter (Whatman). Filters were then floated on 20 ml MM acidified with sulfuric acid to pHs of 0.5 to 6. They were placed in airtight jars and incubated at RT for 16 days with a continuous flow of 45 ml min⁻¹ air containing 10 nmol CS₂ ml⁻¹. Growth at different pHs was determined by measuring colony diameters and counting colonies. The growth of strain BBW1 was quantified visually, as cells had spread over the filter and over the surface of the medium.

**Cell surface hydrophobicity.** Cell surface hydrophobicity was determined by a modified form of the method of Rosenberg et al. (23). The pH of culture samples from the minichemostats was adjusted to 3 or 7 with PUM buffer (23). The suspensions were diluted to an OD₅₀₀ of 0.45 (A₅₀₀) in PUM buffer with the appropriate pH. In a test tube, a 1-ml suspension was mixed with 200 μl n-octane or n-hexane. The mixture was incubated at RT for 10 min, mixed vigorously for 1 min, and left to stand at RT for at least 25 min. OD₅₀₀ was measured (A₅₀₀), and the percent adherence to the solvent was calculated with the equation (1 − A₅₀₀/A₅₀₀) × 100. The use of OD₅₀₀ to measure suspension turbidity yielded similar results.

**Preparation of cell extracts.** Cell extracts from steady-state reactor-grown bacterial cells were prepared as follows. Thirty to 50 ml was removed from the reactors and centrifuged at 4°C for 30 min at 12,000 × g. The cell pellets were washed with 15 ml sterile distilled H₂O and resuspended in 0.5 ml 20 mM KP, at pH 7. Approximately 350 μM glass beads (80- to 110-μm size) were added, and the cells were broken by bead beating for 2 × 2 min at 30 Hz (Retsch) with intermittent cooling on ice. The broken cell mixtures were centrifuged for 5 min at 16,000 × g, and the supernatants were stored at −20°C with a final concentration of 10% glycerol.

**Enzyme kinetics based on H₂S measurements.** The Michaelis-Menten constants Kₘ and Vₘ₉ₐₓ were determined for the CS₂ conversion rates of cell extracts of the different strains by measuring the H₂S production rate with an H₂S microsensor (Unisense) in 20 mM HEPES (pH 7) as described previously (15). Experiments were performed at pH 7, as the CS₂ hydrolyase is predicted to reside in the cytoplasm of the cell because of the absence of a signal sequence at the N terminus of the enzyme. The Kₘ and Vₘ₉ₐₓ Values were calculated from Michaelis-Menten plots by nonlinear regression with the Michaelis-Menten equation V/Vₘ₉ₐₓ = [CS₂]/(Kₘ + [CS₂]). Experiments were repeated at least three times, and average values of three independent experiments ± the standard errors of the means were calculated. The same method was used to determine Vₘ₉ₐₓ Values (with 600 μM CS₂ as the substrate) for steady-state cells from the...
minichemostats \((D = 0.02)\) diluted 200× in reactor medium (MM containing 1% \(\text{H}_2\text{SO}_4\)). Rates were normalized to the reactor OD\(_{600}\).

Sulfur (\(S^0\)) determination. Sulfur was determined by a modified form of the method of Sorbo (24) to reduce interference from medium components and loss of sulfur during processing. Polycarbonate filters (0.1-\(\mu\)m Whatman Cyclopfac track etched membrane 7060-2501 or Millipore Isopore VCTP filters) were rinsed with MilliQ water and placed on a vacuum filter unit. Liquid samples from batch and continuous cultures, as well as bacteria removed from Gelrite plates and resuspended in 0.5 ml sterile demineralized water, were immediately filtered to prevent the bacteria from metabolizing the \(S^0\) before processing. Up to 5 ml culture was carefully loaded directly onto the membrane to prevent \(S^0\) from sticking to the glass of the vacuum unit and filtered under vacuum. Controls consisted of 3 ml MM containing 1% \(\text{H}_2\text{SO}_4\). The filters were rinsed with 1 ml MilliQ water and inserted into a 2-ml Eppendorf tube, and 1.5 ml 0.1 M KCN was added immediately to stop the cells from metabolizing the \(S^0\). The samples were incubated at 90°C for 10 min and cooled to RT, and 200 \(\mu\)l 0.75 M Fe(NO\(_3\))\(_2\) in 20% HNO\(_3\) was added. Samples were centrifuged for 5 min at 16,000 \(\times\) g to pellet precipitate cell debris and filters, and the supernatant absorbance was measured immediately at a wavelength of 460 nm. Standard curves were prepared in the same manner, with a solution of \(S^0\) in acetone (259 mg in 100 ml) diluted in MilliQ water to a final amount of up to 75 \(\mu\)g \(S^0\) per filter.

\(S^0\), \(\text{H}_2\text{S}\), and \(\text{SO}_3^{2-}\) accumulation in bacterial cells. The accumulation of intermediates during CS\(_2\) respiration was measured simultaneously but in separate reaction chambers as follows. Samples from the minichemostats were diluted 10-fold with \(O_2\)-saturated MM containing 1% \(\text{H}_2\text{SO}_4\). The diluted cultures were used to fill three glass cuvettes containing stir bars, after which the cuvettes were closed and placed in a 22°C water bath for 35 min with vigorous stirring. \(\text{CS}_2\) (17 \(\mu\)M) was added to each cuvette, and simultaneous measurements were then made of (i) respiration, (ii) \(\text{O}_2\) production with an \(O_2\) sensor (Unisense), (iii) \(\text{H}_2\text{S}\) production with an \(\text{H}_2\text{S}\) sensor (Unisense), and (iii) \(S^0\) production by following the change in the respiration curve, the total \(\text{O}_2\) consumed \((\Delta A)\) from the chemostat, a 10 \(\mu\)M \(\text{CS}_2\) pulse from a 6 \(\mu\)l stock bottle (see above) was injected into the cuvette. \(\text{H}_2\text{S}\) production and removal, as well as respiration, were measured simultaneously with an \(\text{H}_2\text{S}\) microsensor (Unisense) and an oxygen sensor (Strathkelvin Instruments), respectively.

Nucleotide sequence accession numbers. The 16S ISR sequences determined in this research have been deposited in the GenBank database under accession numbers KC902816 to KC902829 and KC902831.

RESULTS

Enrichment and isolation of \(\text{CS}_2\)-utilizing bacteria. To obtain extremely acidophilic \(\text{CS}_2\)-converting microorganisms, samples from naturally acidic, sulfur-rich environments and from industrial biotrickling filters were incubated in acidified MM and with \(\text{CS}_2\), as the sole energy source. Significant \(\text{CS}_2\) conversion was observed within a few days, and dense cultures were obtained within 2 to 4 weeks of incubation with 1 to 4% \(\text{H}_2\text{SO}_4\). Ultimately, some enrichment cultures showed growth at 6% \(\text{H}_2\text{SO}_4\) (Table 1). This concentration is equal to a theoretical pH of −0.05. Enrichments containing 4 to 6% \(\text{H}_2\text{SO}_4\) (Table 1) were used to isolate 16 pure cultures on Gelrite plates (0.1% \(\text{H}_2\text{SO}_4\)). To reconfirm their acid tolerance, all isolates were successfully transferred to 4% \(\text{H}_2\text{SO}_4\) medium.

Descriptions of growth characteristics on plate cultures and in liquid cultures are given in the supplemental material and shown in Fig. S1 and S2 in the supplemental material. The 16 isolated strains showed distinctly different colony morphologies, ranging from large, dry, white colonies to smooth, shiny, compact colonies. Stationary-phase liquid cultures showed white or yellow aggregates or little aggregation. From the cryo-SEM analysis of surfaces and cross sections of colonies, we conclude that on solid medium, the compactly growing strains produce more extracellular polymeric substance (EPS) than the spreading strains do.

Phylogenetic analysis. All of the new \(\text{CS}_2\)-converting isolates were identified as Acidithiobacillus thiooxidans strains by conventional 16S rRNA gene analysis (data not shown). Improved discrimination was achieved by analysis of the 16S-23S ISR sequences, containing two tRNA genes and three intergenic transcribed spacers (ITS). The total length of the ISR sequences of the \(\text{CS}_2\)-converting isolates varied between 456 and 460 bp, with one exception; isolate BDW2 from the Oy Visko reactor had an ISR of 439 bp (see Table S2 in the supplemental material). Within the ISR, most of the variation in nucleotide composition was observed in the third of the three ITS. Strains BAW3 and BBW1, which originated from two parallel reactors operating at the Loudon factory, were distinctly different with respect to their nucleotide composition, differing by 57 bp and harboring three insertions and three deletions compared with reference strain G8. In a neighbor-joining phylogenetic tree constructed from the 16S ISR sequences of the \(\text{CS}_2\)-converting strains and other \(A.\) thiooxidans strains, strains BAW3 and BBW1 form a distinct cluster within the \(A.\) thiooxidans strains (Fig. 1). Three more clusters could be distinguished, i.e., cluster 2, which did not contain any of the \(\text{CS}_2\)-converting strains; cluster 3, comprising most of the \(\text{CS}_2\)-converting strains and also \(A.\) albertensis, described as a distinct species but phylogenetically indistinguishable from \(A.\) thiooxidans (26); and cluster 4, containing strain S1p from the Solfatara
(Rome, Italy), strain BC6-1, and strain BDW2 from the Oy Visko plant.

**Screening of Acidithiobacillus reference strains for CS₂ conversion.** To check whether CS₂ conversion is a general trait of acidithiobacilli under our growth conditions, we tested four publicly available Acidithiobacillus species. Of these, the three mesophilic Acidithiobacillus species (*A. albertensis* DSM14366, *A. ferrooxidans* DSM14882, and *A. thiooxidans* DSM504 and DSM14887) were not able to convert CS₂ during the 2 to 5 days the cultures were monitored. Since a hierarchical utilization of energy sources may still be possible, CS₂ utilization cannot be completely ruled out. However, the moderate thermophile *A. calidus* 8584 was found to be capable of CS₂ conversion as soon as CS₂ was added to a growing culture.

**Maximum acid tolerance.** The maximum acid tolerance of all 16 isolates in batch cultures was determined by serially transferring the strains to medium containing gradually higher concentrations of H₂SO₄. The maximum H₂SO₄ concentration in which growth could be observed within 2 months was taken as the growth limit of each organism. Table 1 shows that all of the isolated strains were able to grow at 4% H₂SO₄, which corresponds to the highest affinity for CS₂ and produce little sulfur under highly acidic conditions. (Table 2).

<table>
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<th>Sample type and origin</th>
<th>Sample pH</th>
<th>Strain</th>
<th>% H₂SO₄ (vol/vol) Enrichment</th>
<th>Max</th>
<th>Colony morphology</th>
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<tr>
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**Chemostat growth of CS₂-converting *A. thiooxidans* strains 2Bp, Sts 4-3, S1p, G8, and BBW1.** To identify the strains that have the highest affinity for CS₂ and produce little sulfur under highly acidic conditions, 5 of the 16 isolated CS₂-converting *A. thiooxidans* strains were selected for further comparison. Selection was based on sample location, different genetic groups as determined by 16S rRNA analysis (Fig. 1), and different colony morphologies on plates. The five strains were grown in continuous culture under identical conditions in MM with 1% H₂SO₄. The strains had comparable growth yields, as determined by comparing OD, total protein, and total carbon measurements (see Table S3 in the supplemental material). The OD of strain Sts 4-3 was consistently lower than that of the other four strains, probably because of the observed smaller amount of elemental sulfur in the culture. The υₘₐₓ values of the strains growing under these conditions were determined by increasing the medium flow and simultaneously increasing the [CS₂] supplied to the reactors with the same factor (resulting in a constant CS₂ load per milliliter of medium input), up to and beyond the point where S⁰ formation started becoming visible in the reactors. Strains S1p and G8 had slightly higher υₘₐₓ values than the other three strains (Table 2).

**Cell surface hydrophobicity.** The differences in growth characteristics on plates and in liquid culture suggested that there may be differences in the surface properties of the strains. To test this, cell surface hydrophobicity was measured by using adherence to n-octane and n-hexane (23). Strains 2Bp and Sts 4-3 had less hydrophobic cell surfaces than strains S1p, G8, and BBW1 (see Fig. S3 in the supplemental material). On plates, strains 2Bp and Sts 4-3 produced compact, smooth, and opaque colonies versus the dry and spread-out colonies of strains S1p, G8, and BBW1. Similar results were obtained when experiments were performed at pH 7 (see Fig. S3A and B) or 3 (see Fig. S3C and D); therefore, a different response to high-pH shock is not the cause of the differences in surface hydrophobicity observed.

**pH optimum and pH tolerance.** The pH optima of the five selected strains were determined with a floating-filter assay on media with pHs ranging from 0.5 to 6. The pH optima varied among 1 (2Bp), 1.5 (Sts 4-3 and G8), and 2 (S1p) (Table 2). Strain BBW1 did not form colonies but showed spreading surface growth on the filter and the medium as well. On the basis of visual observations, the pH optimum of this strain was between 1 and 1.5 (Table 2).

Tolerance of different pH levels was estimated by counting the colonies that appeared on the filters after the transfer of cells growing at 1% H₂SO₄ (measured pH, 0.72) to media with lower or higher pHs. Survival rapidly decreased when cells were exposed to...
more acid (pH 0.5) and more gradually decreased when cells were exposed to higher-than-optimum pHs. Strain BBW1 was the most sensitive to high-pH stress; no growth was observed in medium with a pH higher than 3.5.

Enzyme kinetic analysis.

To assess the CS2 removal efficiencies of the five new CS2-converting *A. thiooxidans* isolates, the CS2 affinity constants (*Km*) and maximum CS2 conversion rate (*Vmax*) of crude protein extracts from continuous cultures were determined by adding a pulse of CS2 to diluted protein extracts and measuring the rate of H2S production. Table 2 shows that the *Km* values of the five strains are of the same order of magnitude, ranging between 81 and 130 μM CS2 for strains G8 and 2Bp, respectively. Comparison of the *Vmax* values revealed crude extracts from strain S1p to have a consistently higher *Vmax* under these conditions than crude extracts from the other four strains tested, resulting in a 2-fold higher *kcat/Km* value for S1p. In accordance, the *Vmax* for CS2 of steady-state, minichemostat-grown, intact S1p cells was consistently slightly higher than the *Vmax* of the other strains (Table 2).

Sulfur production and consumption. (i) Sulfur production.

Production of S0 by CS2-converting acidithiobacilli as an intermediate in the oxidation of H2S to SO42− can block biotrickling filters and subsequently decrease performance. Therefore, we compared the H2S and S0 production and consumption of the five selected *A. thiooxidans* strains upon CS2 pulses. When concentrations as low as 1.8 μM CS2 (equivalent to 36 ppm CS2 in the gas phase) were added to a cuvette containing diluted samples from the minichemostats, there was an almost immediate increase in S0, just above the detection level. Peak concentrations of H2S ranged from 0.5 to 1.0 μM under these conditions, and so, S0 formation already started at H2S concentrations below this value. In subsequent experiments, H2S and S0 production was measured simultaneously in one cuvette. Addition of 17 μM CS2 resulted in an immediate and large accumulation of H2S for all strains. Also, S0 formation started almost without delay and continued until virtually all of the H2S had been consumed (Fig. 2). The respiration curves show an initial period of fast respiration when H2S is still present, followed by a sudden decrease in the respiration rate when the cells start respiring solely on S0. This decrease in the respiration rate indicates that the processing of the S intermediates in the cell, and not respiration, is the rate-limiting step. This was observed in all of the strains, but it was most prominent in strain Sts 4-3 (Fig. 2). The chemical reaction of H2S with O2 was less than 2 μM H2S h−1 and therefore did not significantly contribute to the observed oxygen consumption rates.

During the period of S0 respiration, we often observed a temporary reduction in the respiration rate. Although it is possible that an intermediate temporarily accumulated that inhibited res-
pation on S\textsuperscript{0}, at this point, the S\textsuperscript{0} consumption rate did not decrease. Also, although detectable levels of the potentially inhibiting intermediate SO\textsubscript{3}\textsuperscript{2-} were present throughout the experiment, there was no increase at the reduced respiration “bump.” Therefore, the apparent temporary reduction in respiration is more likely due to the sensor being affected by an intermediate at that point in the experiment.

At the point where S\textsuperscript{0} peaks, the H\textsubscript{2}S and CS\textsubscript{2} had been completely consumed and only 30 to 40% of the total oxygen was consumed. Therefore, the remaining O\textsubscript{2} consumption resulted entirely from S\textsuperscript{0} oxidation, if the accumulation of any other intermediates is excluded. With this O\textsubscript{2} consumption, and taking into account that this is an underestimate of the actual O\textsubscript{2} consumption because of a small baseline drift upward of the O\textsubscript{2} sensor during the experiment, we calculated that at least 80% of the S added as CS\textsubscript{2} accumulated as S\textsuperscript{0}. This was similar for all of the strains tested (Table 2), and the percentage also remained identical when CS\textsubscript{2} concentrations as low as 1.8 \mu M were added. Below this value, H\textsubscript{2}S formation could not be observed any more, making such calculations impossible.

The rates of S\textsuperscript{0} formation and consumption were calculated from the slopes before and after the apex of the OD\textsubscript{480} trace (Fig. 2). Consistently, S\textsuperscript{0} production (corrected for consumption) was between four times (strains 2Bp, S1p, G8, and BBW1) and nine times (strain Sts 4-3) faster than S\textsuperscript{0} consumption. This matches with a buildup of S\textsuperscript{0} of at least 80% of the total S added, as calculated above from the oxygen respiration. In separate experiments, chemical analysis for S\textsuperscript{0} at the moment OD\textsubscript{480} reached its maximum value consistently showed S\textsuperscript{0} recovery between 60 and 67% (Table 2). Therefore, chemical analysis appeared to underestimate the amount of S\textsuperscript{0} produced during CS\textsubscript{2} respiration. However, both methods of determining S\textsuperscript{0} accumulation upon the application of CS\textsubscript{2} pulses indicated that all of the strains tested produced about equal amounts of extracellular S\textsuperscript{0} under conditions of excess CS\textsubscript{2}.

(ii) Sulfur consumption. Although all of the strains tested behaved similarly in terms of S\textsuperscript{0} production, there were some obvious differences in subsequent S\textsuperscript{0} respiration (Fig. 2); strain Sts 4-3 respired on S\textsuperscript{0} five to eight times more slowly than the other four strains. The H\textsubscript{2}S combined with S\textsuperscript{0} respiration rates (the first part of the respiration curve) showed a maximum 2-fold difference between the strains (Fig. 2 and Table 2). Although strain Sts 4-3 respired more slowly on S\textsuperscript{0}, the respiration rate did not decline until all of the S\textsuperscript{0} had been depleted.

### Table 2: Comparison of CS\textsubscript{2}-converting A. thiooxidans strains 2Bp, Sts 4-3, S1p, G8, and BBW1

<table>
<thead>
<tr>
<th>Characteristic</th>
<th>2Bp</th>
<th>Sts 4-3</th>
<th>S1p</th>
<th>G8</th>
<th>BBW1</th>
</tr>
</thead>
<tbody>
<tr>
<td>Colony morphology</td>
<td>Smooth, domed</td>
<td>Small, smooth, domed</td>
<td>White, dry, compact</td>
<td>White, dry, spreading</td>
<td>White, dry, spreading</td>
</tr>
<tr>
<td><strong>A. thiooxidans 16S ISR cluster (Fig. 1)</strong></td>
<td>3</td>
<td>3</td>
<td>4</td>
<td>3</td>
<td>1</td>
</tr>
<tr>
<td>Maximum acid tolerance (% [vol/vol] sulfuric acid)</td>
<td>5</td>
<td>5</td>
<td>5</td>
<td>4</td>
<td>6</td>
</tr>
<tr>
<td>pH optimum</td>
<td>1</td>
<td>1.5</td>
<td>2</td>
<td>1.5</td>
<td>1–1.5</td>
</tr>
<tr>
<td>pH tolerance</td>
<td>0.5–6</td>
<td>0.5–5</td>
<td>1–6</td>
<td>0.5–6</td>
<td>0.5–3.5</td>
</tr>
<tr>
<td>Cell surface hydrophobicity</td>
<td>Low</td>
<td>Low-intermediate</td>
<td>High</td>
<td>High</td>
<td>High</td>
</tr>
<tr>
<td>Reactor dilution rate at point of S\textsuperscript{0} formation (approaching ( \mu \text{max} ))</td>
<td>0.09</td>
<td>0.08</td>
<td>0.1</td>
<td>0.1</td>
<td>0.09</td>
</tr>
<tr>
<td>Mean cell extract ( K_m (\mu \text{M CS}_2) \pm \text{SEM} )</td>
<td>130 ± 22</td>
<td>97 ± 10</td>
<td>100 ± 5</td>
<td>81 ± 7</td>
<td>116 ± 4</td>
</tr>
<tr>
<td>Mean cell extract ( V_{\text{max}} (\mu \text{M H}_2\text{S} \text{min}^{-1} \text{mg protein}^{-1}) \pm \text{SEM} )</td>
<td>38 ± 3</td>
<td>17 ± 0</td>
<td>48 ± 7</td>
<td>23 ± 1</td>
<td>28 ± 5</td>
</tr>
<tr>
<td>( k_{\text{cat}}/K_m (\mu \text{M}^{-1} \text{s}^{-1}) )</td>
<td>3.5</td>
<td>2.1</td>
<td>6.5</td>
<td>3.4</td>
<td>3.3</td>
</tr>
<tr>
<td>Mean whole-cell ( V_{\text{max}} (\mu \text{M H}_2\text{S} \text{min}^{-1} \text{ml culture}^{-1} \text{for OD}\text{max of 1}) \pm \text{SEM} )</td>
<td>11 ± 0</td>
<td>10 ± 0</td>
<td>12 ± 0</td>
<td>8 ± 0</td>
<td>11 ± 0</td>
</tr>
<tr>
<td>Mean calculated S\textsuperscript{0} accumulated (% of total S pulse added) ( \pm \text{SEM} )</td>
<td>76 ± 4</td>
<td>83 ± 1</td>
<td>82 ± 1</td>
<td>83 ± 1</td>
<td>ND\textsuperscript{b}</td>
</tr>
<tr>
<td>Mean measured S\textsuperscript{0} accumulated (% of total S pulse added) ( \pm \text{SEM} )</td>
<td>67 ± 2</td>
<td>63 ± 2</td>
<td>65 ± 1</td>
<td>61 ± 1</td>
<td>ND</td>
</tr>
<tr>
<td>Mean respiration rate on H\textsubscript{2}S and S\textsuperscript{0} combined after a 10 \mu M CS\textsubscript{2} pulse (nmol O\textsubscript{2} \text{min}^{-1} \text{ml culture}^{-1} \text{for OD}\text{max of 1}) \pm \text{SEM}</td>
<td>45 ± 9</td>
<td>43</td>
<td>87 ± 10</td>
<td>101 ± 1</td>
<td>66 ± 7</td>
</tr>
<tr>
<td>Mean respiration rate on S\textsuperscript{0} only after 10 \mu M CS\textsubscript{2} pulse (nmol O\textsubscript{2} \text{min}^{-1} \text{ml culture}^{-1} \text{for OD}\text{max of 1}) \pm \text{SEM}</td>
<td>41 ± 3</td>
<td>7</td>
<td>63 ± 3</td>
<td>44 ± 1</td>
<td>49 ± 1</td>
</tr>
<tr>
<td>Mean % of S\textsuperscript{0} globules attached to cells after 10 17 \mu M CS\textsubscript{2} pulses ( \pm \text{SEM} )</td>
<td>87 ± 7</td>
<td>17 ± 4</td>
<td>9 ± 2</td>
<td>52 ± 2</td>
<td>22 ± 2</td>
</tr>
<tr>
<td>Mean % of cells attached to S\textsuperscript{0} globules after 10 17 \mu M CS\textsubscript{2} pulses ( \pm \text{SEM} )</td>
<td>35 ± 10</td>
<td>13 ± 3</td>
<td>7 ± 2</td>
<td>30 ± 6</td>
<td>13 ± 0</td>
</tr>
<tr>
<td>Resistance to CS\textsubscript{2} stress</td>
<td>Low</td>
<td>Medium</td>
<td>Medium</td>
<td>Medium</td>
<td>Medium</td>
</tr>
<tr>
<td>Speed of recovery after CS\textsubscript{2} starvation</td>
<td>Slow</td>
<td>Medium</td>
<td>Slow</td>
<td>Fast</td>
<td>Fast</td>
</tr>
</tbody>
</table>

\textsuperscript{a} Strains were grown in continuous culture (D = 0.02) with CS\textsubscript{2} as the sole energy source. Samples were taken from these reactors for the comparison experiments. The \( K_m \) and \( V_{\text{max}} \) of each strain were calculated from Michaelis-Menten plots by nonlinear regression with the Michaelis-Menten equation \( V = V_{\text{max}} \times S/(K_m + S) \). Mean values from at least three independent experiments are shown.

\textsuperscript{b} ND, not determined.
This was in contrast to the other strains, especially strain S1p, which showed a continuous decline in the rate of respiration and concurrent S0 depletion.

We hypothesized that different strains produce differently bioavailable S0; strains 2Bp, G8, and BBW1 produce S0 that can be efficiently metabolized again, whereas strains Sts 4-3 and S1p produce S0 that is difficult to remove. To test this hypothesis, we examined sulfur accumulation by different strains upon the application of repeated CS2 pulses to undiluted chemostat samples by counting S0 globules under a light microscope (Table 2). We counted 160 to 240 cells of each strain, and a representative picture of strains 2Bp, Sts 4-3, S1p, and G8 is shown in Fig. S4 in the supplemental material. All five of the strains tested showed the accumulation of S0 globules of similar sizes, either attached to the bacteria or loose in the medium (see Fig.S4). There were large differences in the observed cell attachment to S0 globules. Although a correlation between the attachment of cells to S0 globules and cell surface hydrophobicity might be expected, we did not observe this despite the fact that all of the cells had identical physiological backgrounds. Strain S1p clearly had the fewest S0 globules that were attached to cells (9% ± 2%), while in cultures of strain 2Bp, most of the S0 globules were attached to cells (87% ± 7%, Table 2). This supports our hypothesis that S1p produces S0 that appears less bioavailable; attachment of S0 globules to bacteria is required for rapid S0 consumption upon H2S depletion. Strain Sts 4-3, which consumes S0 very slowly, also had a low percentage (13%) of cells attached to S0 globules, and 17% of the S0 globules were attached to cells (Table 2). This percentage was not as low as that of strain S1p, and it therefore cannot entirely explain the very low observed S0 consumption rate of this strain. However, strain Sts 4-3 produced more H2S than the other strains when pulsed with CS2 (25 versus 20 μM, Fig. 2), which could have had an inhibitory effect on overall respiration.

**CS2 stress and starvation.** The effect of fluctuations in CS2 concentrations in biofilters can be simulated by applying CS2 pulses to undiluted culture samples from CS2-limited steady-state chemostats in MM with 1% H2SO4. Therefore, chemostat samples of the newly isolated *A. thiooxidans* strains were incubated and subjected to repeated 17 μM CS2 pulses. Each new pulse was given when the H2S produced from the previous pulse had been....

**FIG 2** Conversion of CS2 by five *A. thiooxidans* strains. The arrows indicate the times when 17 μM CS2 was injected into a cuvette containing cells from a continuous culture growing at D = 0.02, diluted 6× in MM containing 1% H2SO4. Respiration (O2 consumption, black dashed line), H2S production (black solid line), and S0 production (gray line) were monitored. The production and consumption rates in these graphs were used to determine the percentages of S0 accumulation in Table 2. Note the different scale on the x axis of the graph for strain Sts 4-3.
consumed by the cells (after about 1.5 to 3 min). The H$_2$S consumption rates after the first CS$_2$ pulse varied between 1.9 (strain of starvation. After 4 h of CS$_2$ starvation, there was only modest to respiratory activity were measured. Results subjected to a CS$_2$ pulse. Subsequent H$_2$S production and con-
reconnected again, samples were taken from the chemostats and
were subjected to CS$_2$ starvation by temporarily shutting down the
supply, the five strains growing in chemostats as described above
and data from a representative experiment are shown as percentages of the H$_2$S consumption rate after the first CS$_2$ pulse. Measurements were done with an H$_2$S sensor, and rates (in nanomoles of H$_2$S per minute per milliliter of
culture) were normalized to a culture OD$_{600}$ of 1.

The observation described above that strain 2Bp suffers more from
CS$_2$ stress than the other four strains do. At 24 h of recovery, the
culture density of all five strains was higher than during steady
state. This indicates that the cultures had started growing and/or
had S$_0$ present.

**DISCUSSION**

Our approach to the enrichment of extremely acidophilic CS$_2$-
converting microorganisms from volcanic regions and CS$_2$-
converting trickling filters proved successful. Conversion of CS$_2$ was
observed within days after inoculation. Furthermore, the enrich-
ments and isolated *Acidithiobacillus* strains could grow at very
high H$_2$SO$_4$ concentrations. The only acidophilic CS$_2$-converting
*Acidithiobacillus* strain described to date, TJ330, was isolated from an
acidic (pH 6.1 to 1.4) CS$_2$- and H$_2$S-treating peat biofilter (9).
The neutrophilic CS$_2$-converting species *Paracoccus denitrificans*
was isolated from oak leaves and soil beneath the leaf canopy (7,
27). Our attempt to enrich acidophilic microorganisms from soil
samples taken under an oak tree and from compost was unsuc-
cessful. Of the *Acidithiobacillus* strains from culture collections
screened for CS$_2$ conversion (at micromolar concentrations), only
*A. caldus* DSM 8584 was positive. This trait was not previously
reported for this species. Our screening confirmed the observation
of Smith and Kelly (28), although they used a potentially toxic
liquid CS$_2$ concentration (2 mM).

The new *Acidithiobacillus* isolates even showed slow growth in
6% H$_2$SO$_4$. The constant supply of CS$_2$ to the cultures was the key

**FIG 3** Effect of repeated addition of CS$_2$ on the H$_2$S consumption capacity of minichemostat-grown cells of *A. thiooxidans* strains 2Bp, Sts 4-3, S1p, G8, and BBW1. Reactor samples were starved for 15 min in a cuvette, and 10 pulses of 17 
µM CS$_2$ were sequentially injected. Strain Sts 4-3 was starved for 15 min before the first injection. The experiment was repeated three times independently, and data from a representative experiment are shown as percentages of the H$_2$S consumption rate after the first CS$_2$ pulse. Measurements were done with an H$_2$S sensor, and rates (in nanomoles of H$_2$S per minute per milliliter of
culture) were normalized to a culture OD$_{600}$ of 1.

**FIG 4** Effects of CS$_2$ starvation and recovery on respiration rates ± the standard error of the mean (n = 3) on internally produced H$_2$S and S$_0$ (A) and on only S$_0$ (B) after a CS$_2$ pulse. The experiment was performed with five CS$_2$-
converting *A. thiooxidans* strains (2Bp, Sts 4-3, S1p, G8, and BBW1), all growing simultaneously in five identically run chemostats. Rates are given in nano-
moles of O$_2$ per minute per milliliter of culture. Note that the respiration rates of strain 2Bp were monitored only at steady state, after 24 h of starvation, and after 4 h of recovery.
factor in the maintenance of cultures at these very high H₂SO₄ concentrations. Culture activity decreased dramatically upon storage without a substrate at or above 4% H₂SO₄. Acidophiles require a continuous and high supply of maintenance energy to be able to actively pump out protons that leak from the acidic environment into the nearly neutral pH cell cytoplasm (29). Operation of biofilters under highly acidic conditions therefore puts additional stress on the microorganisms during periods of fluctuating CS₂ concentration and factory shutdown.

Although growth was very slow at 6% H₂SO₄, dense growth was already observed at 4% for all new Acidithiobacillus strains. Similar H₂SO₄ tolerance was reported for Acidithiobacillus sp. strain AZ11, which is able to respire on elemental sulfur in the presence of 4.2% H₂SO₄ (30). The pH optima determined for 5 of the 16 new CS₂-converting strains were between 1 and 2. This is slightly lower than the optimal-pH range of 1.8 to 2.5 described for other Acidithiobacillus strains (29, 31).

Growth at around pH 0, as observed for 15 of our A. thiooxidans isolates, is among the lowest pHs reported in the literature for any organism. Ferroplasma acidarmanus (32), Picrophilus oshii-mae, and Picrophilus torridus could grow at pH 0 (optimum pH, 0.7) (33). Picrophilus torridus adapted to growth at pH 0.1 even showed significant growth at 1.2 M H₂SO₄ (pH −0.06) (34). The euarkotrophic red alga Cyanidium caldarium was cultured at 0.5 M H₂SO₄ (35), and the green alga Dunaliella acidophila is able to survive pH 0.2 (36). Also, some fungal species were reported to grow at pH 0, i.e., Acontium cylatium (37), Cephalosporium sp., and Trichosporon cerebrae (38). We also observed fungal growth at 6% H₂SO₄ (pH −0.05) in our enrichment cultures but did not further investigate the species present in these cultures. With growth at pH as low as −0.05 (6% H₂SO₄), the new Acidithio-bacillus isolates obtained in this research exceed the previously reported pH limit of 0.5 for microbial CS₂ conversion for Acidithio-bacillus TJ330 (9).

The newly isolated CS₂-converting A. thiooxidans strains differed in colony morphology. The genus Acidithiobacillus comprises a physiologically and genetically heterogeneous group of microorganisms (39, 40), despite the often low sequence diversity in the 16S rRNA gene. For that reason, the 16S-23S ISR is used to discriminate at the intra species level (41, 42).

Two main colony types on Gelrite plates were distinguished, compact, creamy, shiny colonies and dry, white, spreading colonies (40). Reversible variation in colony morphology of several A. ferrooxidans strains has been described, resulting in the same large, white spreading colonies, as opposed to compact colonies, as observed here for some of the newly isolated A. thiooxidans strains (43, 44). A. thiooxidans strains may be motile via a polar flagellum (40). A. ferrooxidans ATCC 19859 spreading variants displayed increased motility and chemotaxis toward thiosulfate, which may be a selective advantage over biofilm growth during periods of low substrate concentrations. These variants arose through the rearrangement of insertion sequences in the genome, potentially acting as a genetic switch (44). The A. ferrooxidans group of strains has recently been reclassified into four separate species (45). Of these, only A. ferrivorans and some A. ferrodurans strains were shown to be motile (45). The type strain A. ferrooxidans ATCC 23270 lacks flagellum and chemotaxis genes (46). The draft genome of A. thiooxidans ATCC 19377 (47) and the draft genomes of both A. thiooxidans strains S1p and G8 (Daan Speth, personal communication) do contain the operons for flagellum biosynthesis and chemotaxis. However, we did not observe swimming motility in liquid cultures of our strains when we examined them microscopically. Therefore, the mechanism and role of the spreading colony phenotype in these strains are not clear.

SEM studies of frozen colonies indicated that the difference in colony appearance may be caused by the absence of a clear EPS layer on the dry white colonies, as has been observed for colony morphology mutants of Mycobacterium smegmatis (22). In support, A. thiooxidans strains S1p, G8, and BBW1, which produced white dry colonies, had a considerably higher cell surface hydrophobicity than strains 2Bp and Sts 4-3, which produced compact shiny colonies, suggesting the presence of relatively more hydrophobic compounds on the cell surface of the latter strains. Acidithiobacillus strains produce EPS containing both neutral sugars and fatty acids (48, 49), the proportion varying depending on the substrate the cells are grown on (50, 51). The EPS of A. thiooxidans grown on S⁰ consists of 40% sugars and 60% fatty acids (mainly eicosanoic acid) (50). The fatty acids are released from the outer membrane by blebbing (52) and cause the “wetting” of sulfur particles described in 1961 by Jones and Starkey (53), making S⁰ available as an energy source. In addition, EPS is essential for successful attachment and bioleaching of A. ferrooxidans to pyrite (50). Differences in EPS production and potential motility observed in our strains may have implications for the degree of colonization and clogging of biofilters.

Efficient biofiltration of CS₂-contaminated air streams requires microorganisms with a higher affinity for CS₂ than the concentration present in the air stream, to ensure its removal to concentrations complying with increasingly stringent regulations, as well as resistance to changes in operating conditions, low biomass production, low S⁰ accumulation, and rapid S⁰ removal to prevent clogging of the biofilters. The affinities of the five strains tested for CS₂ were similar (around 100 μM) and correspond to that reported for the purified CS₂ hydrolase of Acidithiobacillus A1-3 (10). Comparison of the Vₘₐₓ values revealed strain S1p to have a consistently higher Vₘₐₓ under these conditions than the other four strains tested, possibly because it has a relatively larger amount of CS₂ hydrolase present in the cells than the other strains (15). The Vₘₐₓ is only reached at substrate concentrations of 200 μM (nmol ml⁻¹) or higher. Bioreactors treating CS₂-contaminated air from the viscose industry are operational at much lower concentrations of around 4 to 20 nmol ml⁻¹ (100 to 500 ppm) (2), indicating that although strain S1p converts CS₂ with a higher Vₘₐₓ than the other strains, it would not usually reach its full potential reaction rate in a bioreactor. Indeed, a higher Vₘₐₓ may even be deleterious, as it might cause H₂S to accumulate to toxic levels in the cell more rapidly upon CS₂ peaks.

Comparison of the resistance to changes in operating conditions in the form of an interruption in the CS₂ supply revealed that all five strains were affected by 24 h of CS₂ starvation in terms of the ability the respite after a CS₂ pulse during starvation, but they all recovered within 24 h after reconnection of the CS₂ supply. However, during recovery, all five strains will also produce S⁰, as we found in all of the strains tested that CS₂ pulses during starvation resulted in the transient accumulation of 80% of the total S added as S⁰, independently of the amount of CS₂ added. This implies that it will be difficult to avoid S⁰ accumulation in biofiltration systems with uneven CS₂ loading. However, differences in S⁰ removal were observed, with strain Sts 4-3 having a much lower but constant S⁰ removal rate than the other strains and strain S1p...
having a long period in which the S\textsuperscript{0} respiration rate slowly declined. Whatever the cause, the strains that remove S\textsuperscript{0} more slowly will cause more clogging problems in bioreactors because of S\textsuperscript{0} accumulation.

In summary, we have successfully isolated extremely acidophilic, CS\textsubscript{2}-converting \textit{A. thiooxidans} strains from both environmental and industrial ecosystems that grow optimally around pH 1 to 2 and can grow at sulfuric acid concentrations of up to 6% (vol/vol). Currently bioreactors are operated at pH 0.5 to 1 (2). Use of the new strains would reduce water use and improve the prospect for reuse of the produced sulfuric acid in the rayon/viscose industry. The isolated strains displayed different growth and colony morphology characteristics, which may be due to differences in motility and/or the presence or absence of an EPS layer surrounding the cells. To circumvent the bottlenecks in the biofiltration of CS\textsubscript{2}, cocultures of extremely acidophilic \textit{A. thiooxidans} strains to combine the best acid tolerance, affinity for CS\textsubscript{2}, S\textsuperscript{0}-removing potential, and stability during periods of fluctuating CS\textsubscript{2} loads are most promising for inoculation of industrial biofilters. This application is expected to result in reduced sulfur accumulation, increased CS\textsubscript{2} removal rates, reduced water consumption, a more stable operation, and recycling of the sulfuric acid produced.

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